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**New options for nutrient recovery:
Ammonium adsorption and its sequential recovery
by air-stripping or membrane technique**

WaterPro

Kiertotalouden uudet prosessit veden
ja jäteveden käsittelyssä

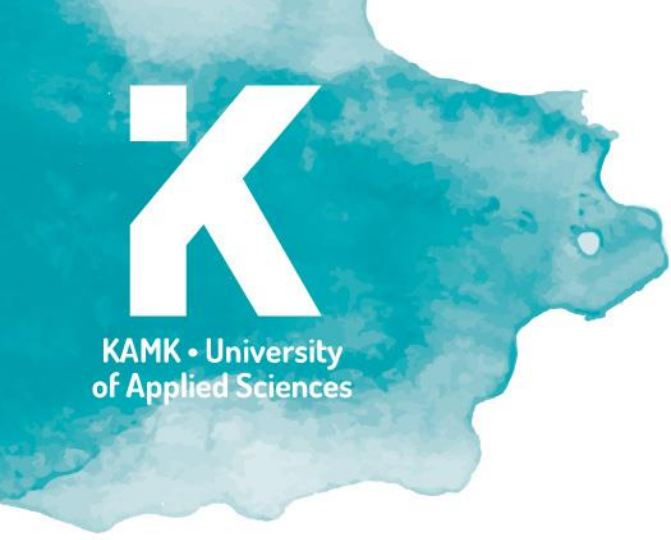
November 2020

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Leverage from
the EU
2014–2020



Laboratory of Applied Geopolymer Technology

Kajaani University of Applied Sciences, Finland

Sustainable construction and civil engineering solutions

Tailing pond construction and management

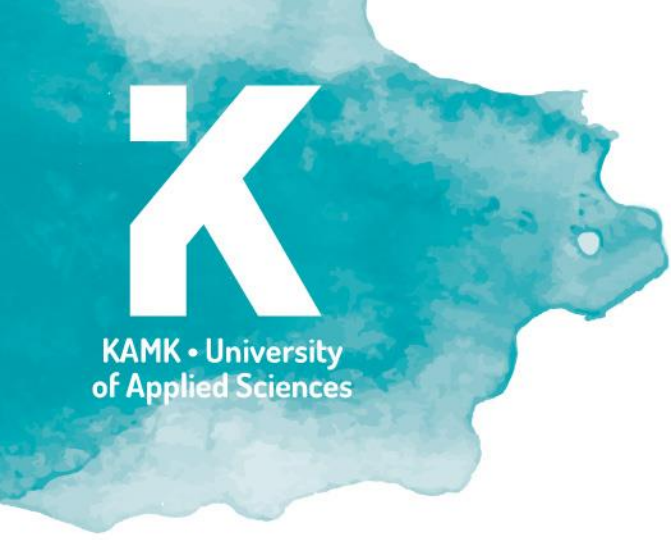


Tailing characterization

Potential of hazardous waste
and tailings encapsulation

Recycling of gangue, bedrock,
tailings in concrete production
and road construction





Laboratory of Applied Geopolymer Technology

Kajaani University of Applied Sciences, Finland

Environmental and water management
in mine industry

Water and waste water treatment applications
(toxic metal(oid)s – removal and/or recovery)

Citizen science and participatory observation



Biogas purification techniques

Nutrient recovery approaches





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European Union
European Regional
Development Fund

Work package 1

Industrial by-
products/side
stream
materials
characterization

Work package 2

Electrochemical
and chemical
precipitation:
nutrients,
sulfates, metals

Work package 3

Removal and
recovery of
contaminants
(lab-scale)

Work package 4

Regeneration or
stabilization
exhausted
materials

Work package 5

Technical
solutions for
wastewater
treatment and
developed
materials piloting

Leverage from

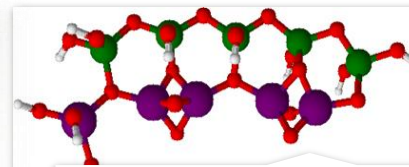
the EU
2014–2020



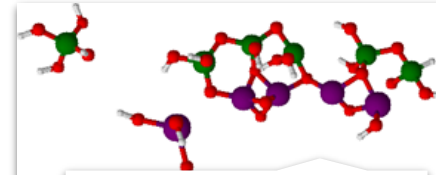
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Geopolymer preparation

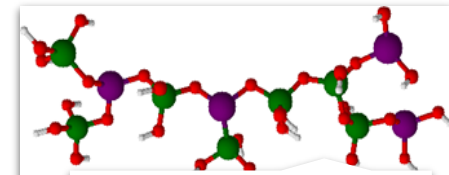
Crashed or powder form



raw aluminosilicate

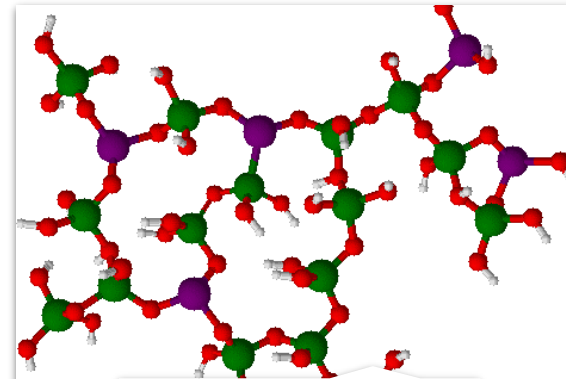


activation



gel phase

Granulated form

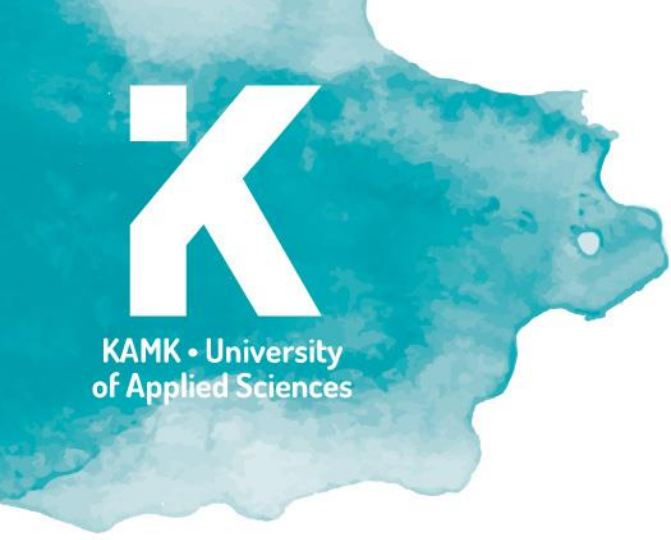


geopolymer



Bulk geopolymer





Raw materials for geopolymerization approach

Waste-to-value
concept

Circular Economy
and green mining

Clays and minerals

Calcinaed materials



Metakaolin



Dolomite/magnesite

Industrial waste streams



Ashes



Pulp sludges



Mine tailings

Industrial by-products



Blast furnace slag
(BFS/BOF)



Silica fume



Design of cost-effective adsorbents

Commercial adsorbents:

Activated carbons (PAC/GAC)

1200-3000 EUR/ton

GHG emission; energy demand;
loss of adsorbent on reg. stage;
utilization problems

Ion-exchange resins (polymers)

1700-3000 EUR/ton

energy demand; organic solvents;
utilization problems

Zeolites (natural minerals)

600-1500 EUR/ton

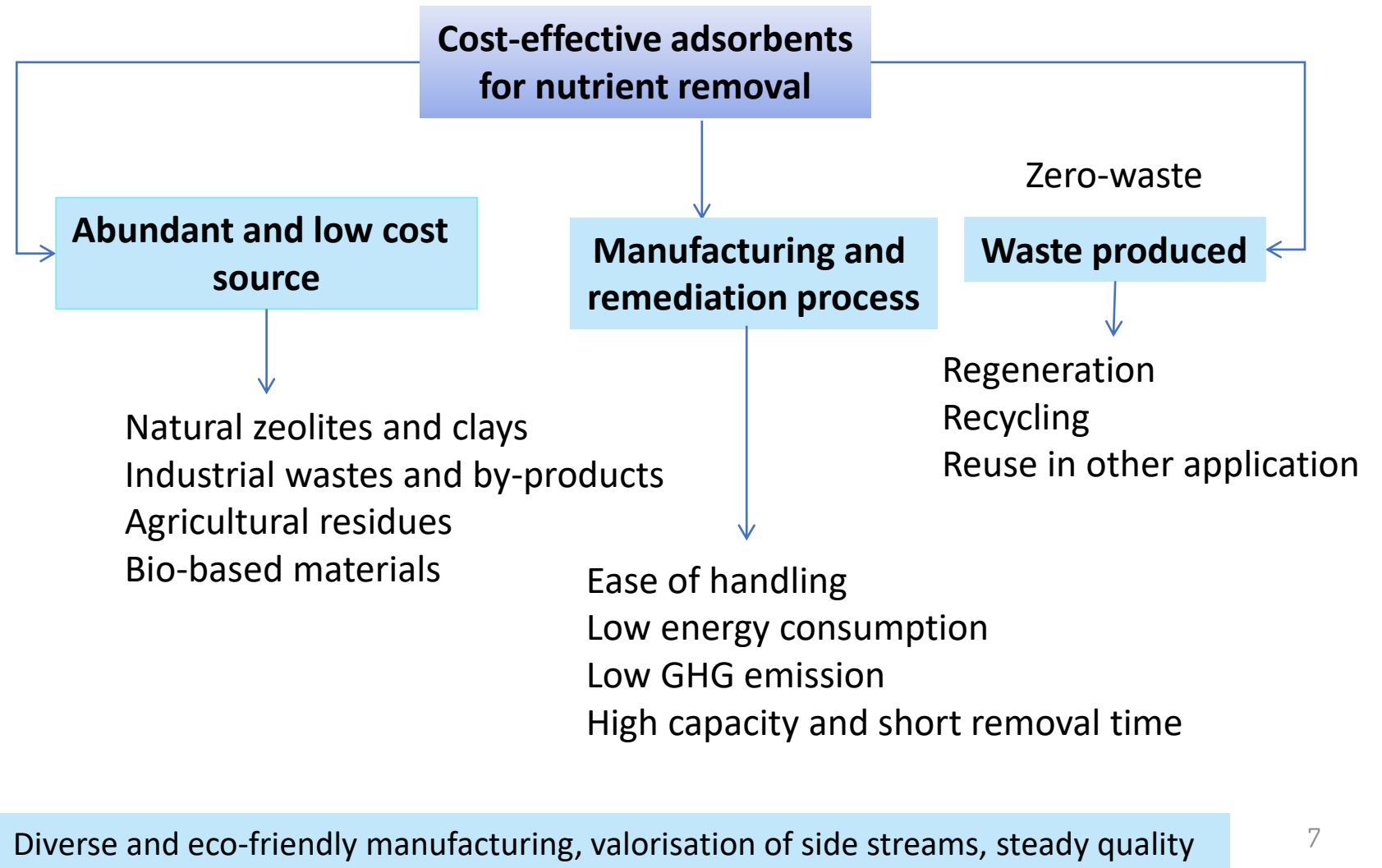
unsteady quality; limit abundances

Sands, gravels, etc.

50-350 EUR/ton

low capacity and nonspecific treatment

Geopolymers 150-300 EUR/ton





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Drivers of nutrient removal and reuse technology

NEED

- Fertilizer production is energy-consuming process
- Discharge of nutrients to natural waters cause eutrophication problems
- Nitrogen load in sewage systems **25 000 ton/a** (Finland) and **60%** of it is removed and lost in current treatment processes
- Decrease of GHG emission
- **Recovery** could be valuable in near future
- Environmental limits for nutrients discharge

SOLUTION

- New geopolymers adsorbent from low-cost sources: unique properties and steady quality
- Combination of mature techniques:
Adsorption → **Air-stripping** → **Absorption**
Evaporation and concentration of final products
Capture in structure and stabilization

BENEFITS

- Technology for nutrient removal from low-laden or diluted streams: **variety of applications**
- Decreases expenses for **aeration** (conventional anaerobic treatment process) or final/polishing treatment
- Small dimensions and ease of integration
- Final product:
raw materials, advanced adsorbents, soil improvers or fertilizers

COMPETITION

- Biotreatment **AMMONOX** (Netherlands) – nitrogen removal only
- **RAVITA/NPHarvest** (Finland) – reject water and digestate, recovery of ammonium
- **ReNOx** (Austria) – natural zeolite adsorbents
- **RemNut** (Italy) – ion-exchange resins
- **Struvite precipitation** – nutrient ratio and Mg source

Sources of undesired nutrient emission

Nutrient-contaminated streams

Low-laden – 10 – 100 mg N/L

Agriculture, fishery, and forestry

- Run-off and storm waters
- Facultative lagoons
- Air purification cattle farms
- Overfertilized fields
- Aquaculture operations
- Ditches and peat bogs

Nutrient close-loop
concept
and
Environmental risk
mitigation

N-P-K



High-laden – 100 – 5000 mg N/L

Municipal and industrial waste-
and processing waters

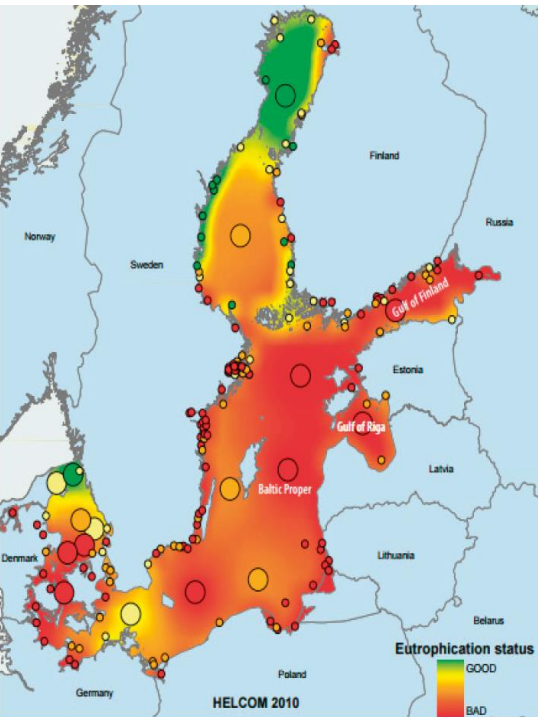
- Sludge digestates
- Dewatering streams of WWTP
- Reject waters of biogas stations
- Landfill leachates
- Textile industry processing waters
- Paper mills grey waters
- Food industry (meat and beverage)

“Urban mining”
concept

POSSIBLE BUSINESS CASES



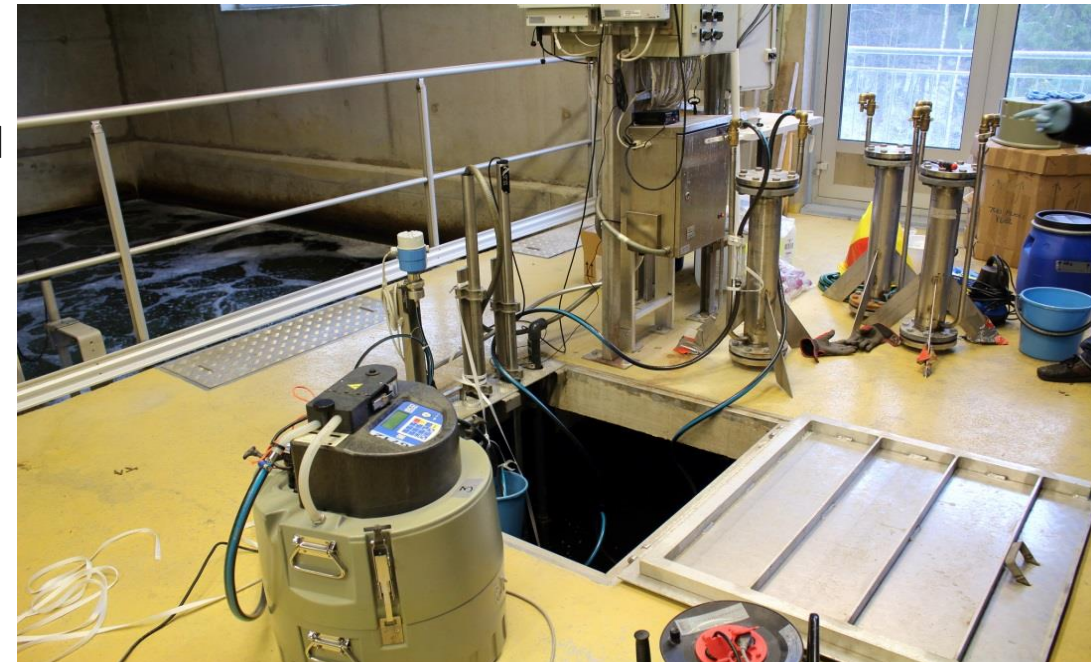
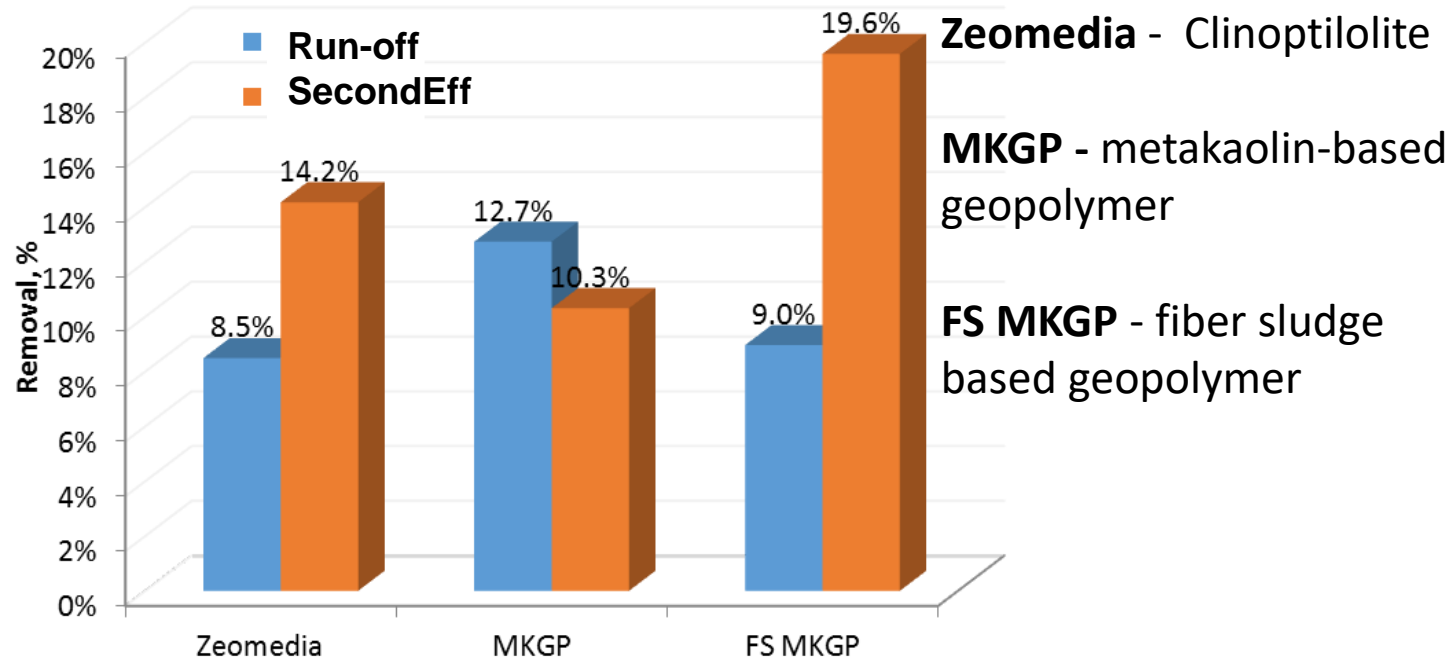
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Helsinki Commission
Baltic Marine Environment
Protection Commission (2010)

Real cases: wastewater treatment of municipal wastewater and mine drainage

Element	Industrial run-off water, mg/L	Secondary effluent, mg/L
Na	163	n/d
Ca	614	27
Mg	14.2	4.4
K	130	0.2
NH ₄ -N	36	31



Enrichment factor up to **20** were reached for industrial run-off waters, and up to **100** for WWTP effluents

Fixed bed column experiment: Adsorption and Regeneration

Adsorption:

Grain size

Flow rate

Temperature



Operation under arctic condition:
Same efficiency at 4°C and 20°C

EBCT was different for synthetic
and real waters

Process easy to handle and maintain

Regeneration:

Regenerants:

Na-salts and K-salts

Chloride, sulfate, phosphate

Conditions:

Regenerant concentration

Alkalinity

Flow rate

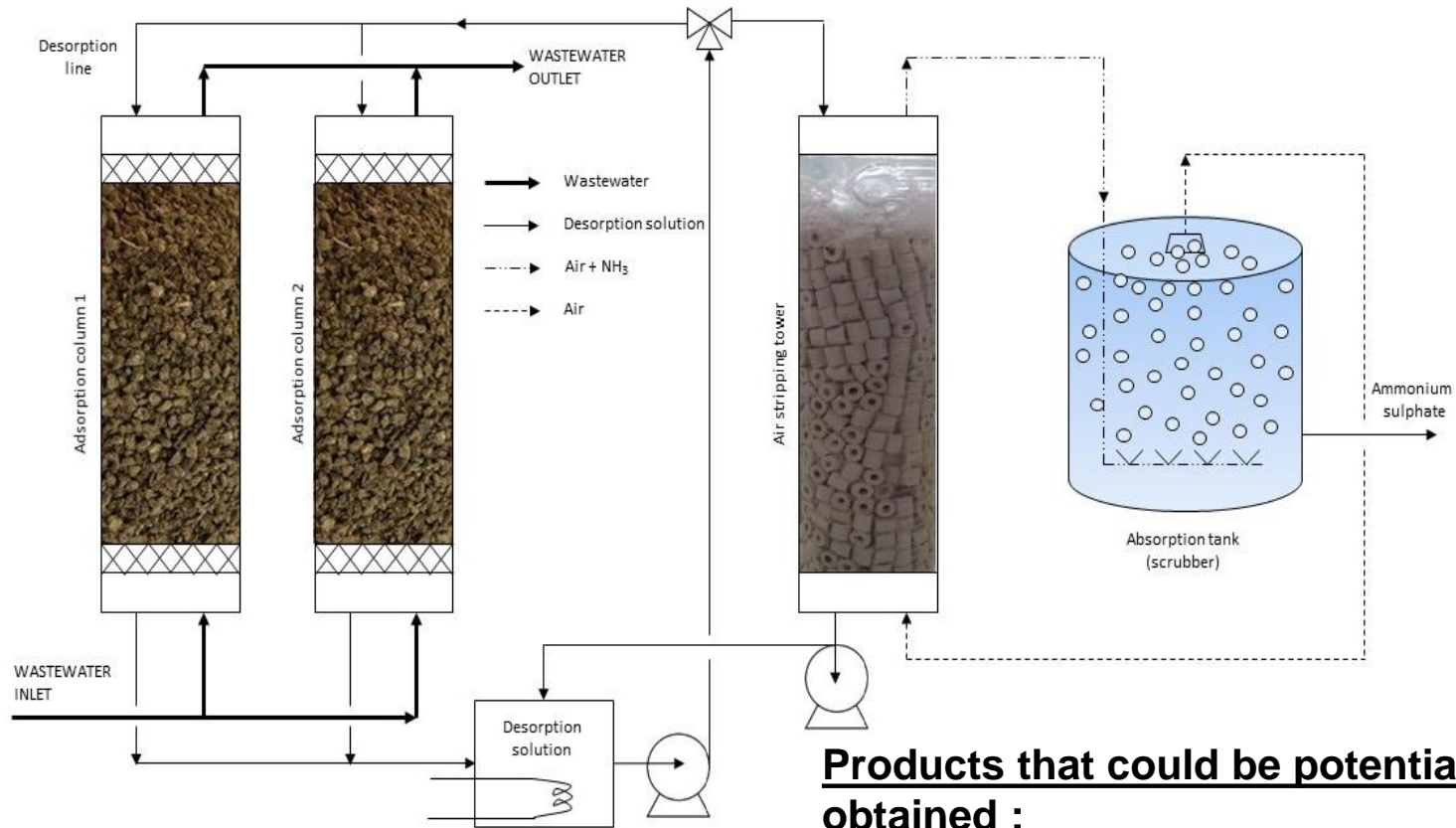
The higher concentration of salt
used, the higher enrichment factor

Low-cost regenerant could be used:
5M NaCl at pH 12

K-salts reduced removal ability
of FS MKGP by 55%

Up to 10 cycles of adsorption-regeneration with a decrease in efficiency of only 15%

Air-stripping experiments and ammonium recovery

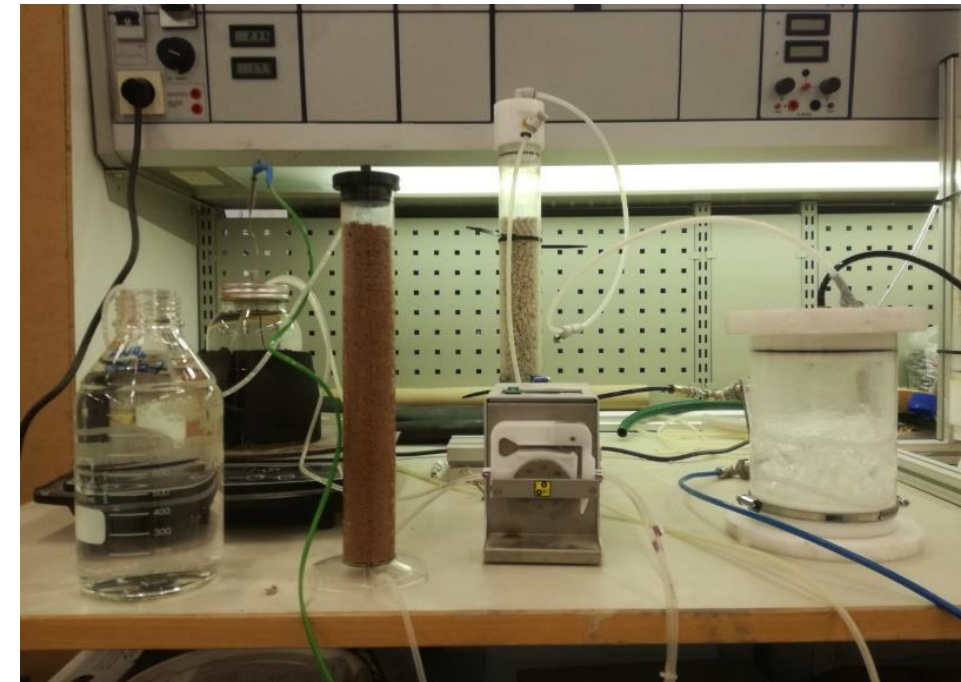


Products that could be potentially obtained :

- Ammonia water (5% NH₄OH)
- Anhydrous ammonia (25% NH₄OH)
- Liquid ammonium sulfate

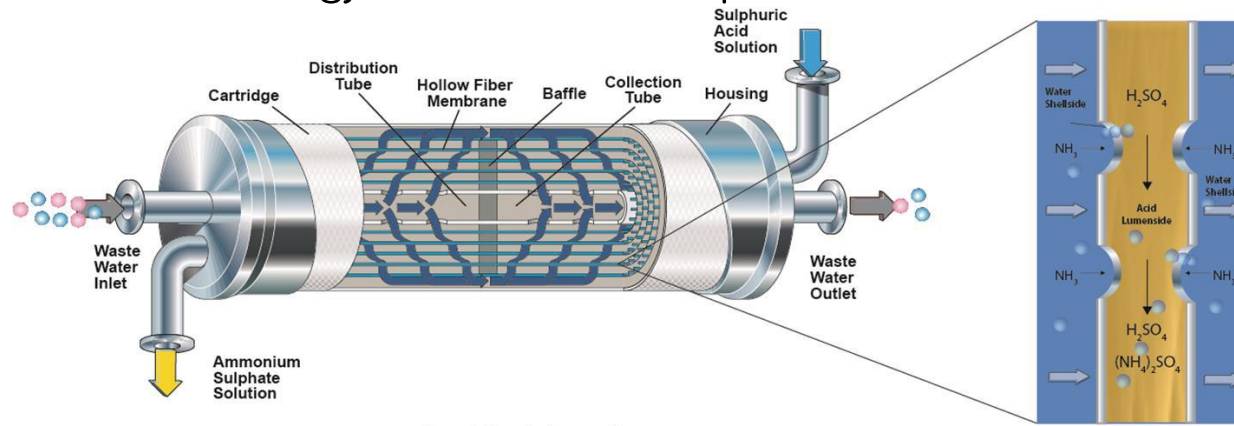
Temperature $45 \pm 5^\circ\text{C}$ was enough to reach conversion rate 91 %.

After the regeneration solution was purified, it was used over 5 times for desorption procedure.

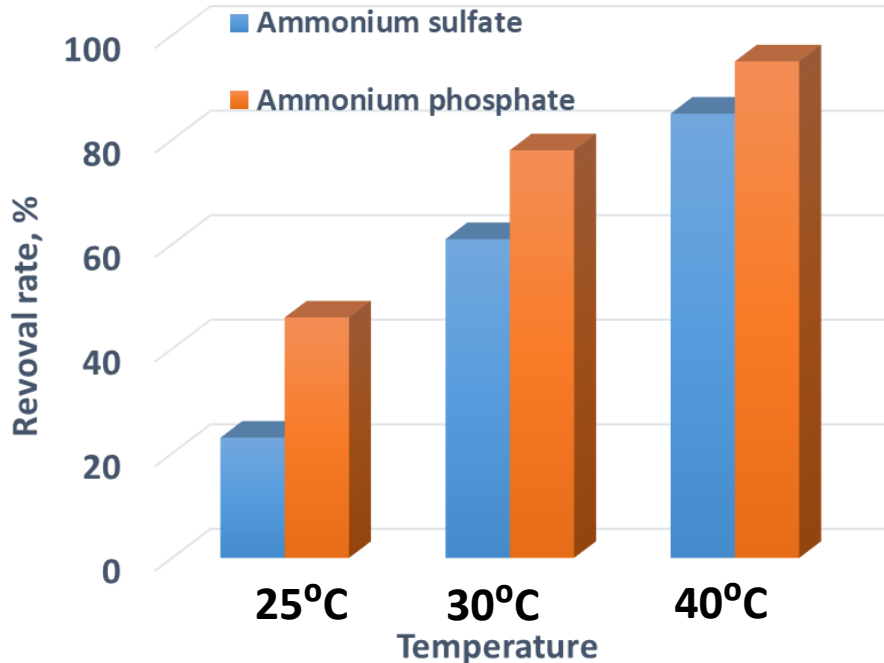


Recovery of ammoniacal nitrogen Transmembrane Chemical Absorption

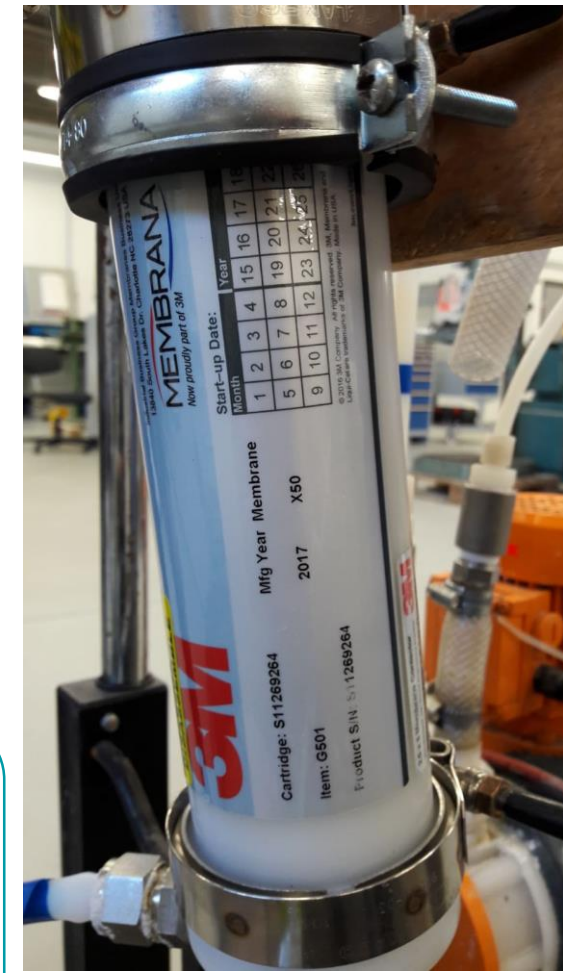
- 3M Liqui-Cel® membrane contactor
- Technology still under development



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The concentration of ammonium-content salt in a resulting received phase were 17% and 22% for phosphate and sulfate salt, respectively.



Conclusions:

Leverage from
the EU
2014–2020

A74635 EAKR, Keski-Pohjanmaan
Liitto/Kainuun Liitto/Pohjois-
Pohjanmaan liitto.



NEXT STEPS

- **Decrease substantially CAPEX**
- **Economical evaluation and LCA**
- **Construction of piloting mobile treatment unit**



Conclusions:

Conventional system is biotreatment in aerobic basins

- Aeration – up to 60% of WWTP energy
- Odor and sludge
- Low temperature is a problem
- We **not recover N**, we have lost it!
- Source of carbon needed (methanol/acetic acid) in polishing step



Innovation approach
is **RECOVERY** of the valuable resource

- Smaller footprint
- Less GHG emissions
- Better water quality
- Possibility to reduce energy consumption and chemicals
 - Getting valuable products to cover expenses

AMMONNOX - 3€/ N kg

Conventional air stripping - > 6€/ N kg

NutriCON (KAMK) - 4.5 €/ N kg **AIM - 1.5-2 €/ N kg**

Conclusions:

- **Adsorption has great potential as remediation technique under arctic condition.**
- **The capacity tests for adsorbent should be repeated with the water being treated. The capacity of the adsorbent granules used in the calculations may be lower than actually used.**
- **It has now been found in laboratory and pilot experiments that regeneration is possible at least 20 times without significant decrease of capacity even for complex matrices.**
- **Nitrogen could be recovered as valuable industrial and agricultural products.**
- **Phosphorous could be removed effectively and potentially recovered locally as soil improver.**



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